ACTIVATION OF C-H BONDS IN SATURATED HYDROCARBONS. THE CATALYTIC FUNCTIONALI-SATION OF CYCLOOCTANE BY MEANS OF SOME SOLUBLE IRIDIUM AND RUTHENIUM POLYHYDRIDE SYSTEMS

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Summary.- Homogeneous catalytic dehydrogenation of cyclooctane into cycloöctene has been effected by means of a variety of iridium and ruthenium polyhydrides, at 150°C, in the presence of an olefin as the hydrogen acceptor; best results (45-70 catalytic turnovers) have been achieved with $(iPr_3P)_2IrH_5$, $[(p-F-C_6H_4)_3P]_2IrH_5$ and $[(p-F-C₆H_A)_zP]_zRuH_A$.

Heterogeneous reactions (reforming, hydrocracking) involving alkanes, used on a large scale industrially, require vigorous conditions and are very unselective.¹ Homogeneous transition metal catalysts are often milder and more selective than their heterogeneous counterparts, $\frac{1}{2}$ and current interest³ in the "activation" of saturated hydrocarbons by soluble transition metal compounds is sustained by the prospect of finding a system which would allow the efficient, selective, catalytic, functionalisation of these rather unreactive substrates. Although a few soluble systems (containing Pt, 4 Ir, 5 Re, 6 Rh, 7 Lu and Y^8) have recently been discovered which bring about the insertion of the transition metal into the C-H bonds of saturated hydrocarbons, in only one case has such a reaction actually led to catalysis: cycloalkenes are formed catalytically from cycloalkanes when these are treated with the bisphosphine rhenium heptahydrides $(\text{Ar}_3\text{P})_2$ ReH₇ (1a) and an olefin (e.g., λ) as a hydrogen acceptor.^{6b,9}

We imagine that this homogeneous catalytic dehydrogenation proceeds by the mechanism shown in the Scheme, 10 via highly reactive 14e intermediates such as \$2 (which may exist in equilibrium with cyclometalled intermediates), and that the maximum number of catalytic *turnovers* which can be achieved [about 10 in the reaction involving cyclooctane and $1a$ (Ar = p-F-C₆H_A)] is limited by competition between the C-H insertion step $(4a \rightarrow 5a)$ and various deactivation processes $[e.g.,$ oligomerisation or further dehydrogenation (by ζ) of the 14e intermediates 4al.

We were interested to find out whether other soluble 18e transition metal polyhydride systems, which should be capable of affording reactive 14e intermediates $\frac{4}{3}$ in the same way (see Scheme), would also convert alkanes into alkenes. We hoped we might find a system which would deactivate less readily and thus lead to a greater number of catalytic turnovers.

Scheme. Postulated catalytic cycle for the dehydrogenation of saturated hydrocarbons by soluble 18e transition metal polyhydrides 1 . $[M] = \mathfrak{g}$, $(\text{Ar}_{\mathcal{I}}P)$ ₂ReH₃; \mathfrak{g} , $(1Pr_{\mathcal{I}}P)$ ₂IrH; \mathfrak{g} , $(1P^{-}F^{-}G_{6}H_{4})$ ₃P₁₂IrH β , (Me₃P)₂IrH; β , L(p-F-C₆H₄)3PJ₃Ru; ζ , (Ph₃P)₃Ru.

We have therefore examined the reactions of a variety of ruthenium and iridium polyhydrides with cyclooctane,¹¹ and found that the iridium pentahydrides (iPr₃P)₂IrH₅ (1b) and [(p-F-C₆H₄)3P12IrH₅ (1c)¹³ and the ruthenium tetrahydride [(p-F-C $_{6}$ H $_{4}$) $_{7}$ P] $_{7}$ RuH $_{4}$ (1e) $^{\circ}$ are indeed more effective catalysts than the rhenium heptahydride λ (Ar = p-F-C₆H₄) for the dehydrogenation of this cycloalkane. Deoxygenated solutions of the polyhydrides $\iota\!$, $\iota\!$, $\iota\!$ and $\iota\!$ (2 mM) and 3,3-dimethylbutene (2) (200 mM) in cyclooctane were heated at 150°C in evacuated sealed tubes¹⁵ until no further reaction occurred. The iridium pentahydride $1\hbar$ gave 23 catalytic turnovers after 3 hours and reached a maximum of 70 turnovers (<u>i.e</u>., 70 moles of cycloöctene¹⁶ were formed per mole of $\downarrow\!\!\!\downarrow$) after 5 days; the ruthenium tetrahydride 2.6 gave 45-55 turnovers after 10 days; and the iridium pentahydride $\int_{\mathcal{L}}$ gave 30-35 turnovers after 5 days. When the initial quantity of olefin ζ was halved ($\zeta \zeta$ 2 mM, and ζ 100 mM), after 8 days it was almost entirely converted to $2,2$ -dimethylbutane (g.c.) and 45 moles of cyclooctene per mole of $\int_{\mathcal{L}}$ were formed (corresponding to a yield of 90% with respect to \mathfrak{z}). Presumably \mathfrak{z} and cyclooctane compete for the reactive intermediate capable of inserting into a C-H bond of cyclodctane.

The polyhydrides (Me₃P)₂IrH₅ (1d)¹⁷ and (Ph₃P)₃RuH₄ (1d)¹⁸ also catalysed the formation of cyclooctene'' from cyclooctane under the same conditions but they were less effective than $\iota\!$, $\iota\!$, $\iota\!$ and $\iota\!$.

The solutions were colourless (λ_k) , yellow (λ_k, λ_k) , or orange (λ_k, λ_k) at the start of the reactions, and brown at the end. They appeared to be perfectly homogeneous throughout, and the presence of mercury did not significantly

affect the yields of cyclooctene, indicating that colloidal metal was not involved.²⁰ Furthermore, samples of the ruthenium tetrahydride le, recrystallised from different solvent systems, 21 were equally effective as catalysts, sug gesting that the catalytically active species is derived from the tetrahydride rather than from a trace impurity.

This approach to the catalytic dehydrogenation of cycloalkanes thus appears to be quite general. We believe that systems such as 1, which are capable of forming 14e intermediates (see Scheme), are more likely to lead to efficient catalysis than systems involving only 16e intermediates. Not only are 14e complexes expected to be more reactive than related 16e complexes in the key C-H insertion step (e.g., $A \rightarrow \Sigma$), but catalysis requires the regeneration of a reactive intermediate, and this can be achieved when the product of the C-H insertion step is itself still coordinativcly unsaturated (16e) and therefore able to undergo further reaction (e.g., β -elimination, followed by loss of olefin, $5 \rightarrow 6 \rightarrow 2$). ²²

References and Footnotes

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- 3. The presence of a hydrogen acceptor is necessary, for thermodynamic reasons, in catalytic dehydrogenations, since the reaction: alkane \rightarrow alkene + H_2 is endergonic.
- 11. We have mainly used cyclooctane as the substrate since it has a convenient boiling point (lSO'C), and it gave the best results with the rhenium systems; \mathbf{u} it contained no detectable cyclooctene (< 2 ppm by g.c.).
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- 13. \lg (prepared by the method described for "(Ph₃P)₂IrH₃" by L. Malatesta, G. Caglio, and M. Angoletta, J.Chem.Soc., 1965, 6974, except that LiAlH₄ in THF was used in the reduction step instead of NaBH₄ in MeOH): ¹H nmr (CD₂C1₂) 6 (from TMS) 7.4 and 7.0 (m, Ar-H) and -9.05 (t, $\frac{1}{\mu}$ = 13 Hz, Ir-H); $\frac{31}{P}$ {Ar-H} nmr (CD₂Cl₂), δ (downfield from external H₃PO₄) 10.04 (sextet, \underline{J} = 13 Hz). 14. le (prepared in the same way as $1f^{18}$): $1f^{18}$ $1f^{18}$ nmr (C_6D_6) , 8 (from TMS) 7.3 and 6.6 (m, Ar-H) and -7.5 (m, Ru-H).
- 15. Preliminary experiments carried out in Schlenk tubes at or near the reflux temperature under an atmosphere of argon gave erratic results, presumably because of the volatility of the olefin 3.
- 16. The yields of cyclooctene were determined by $g.c.$ (silicone SE30 column). The olefin was isolated as its $AgSbF_6$ salt and identified by its mass spectrum except in the reaction involving 1e in which cyclooctene was identified by $g.c.-m.s.$
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- 21. The ruthenium tetrahydride $\int_{\mathcal{R}}$ was recrystallised from either benzene and MeOH or ether and hexane. From the latter solvent system 1e crystallised as $[(p-F-C_6H_4)3^P]_3RuH_4.3/4 C_4H_{10}$ ^O (confirmed by ¹H nmr).
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